## AMENDMENTS TO THE SPECIFICATION

***Please replace the paragraph on page 8, lines 10-11, with the following:***

~~Fig. 3 is a dot graph~~ Figs. 3(a) and 3(b) are dot graphs illustrating change with time of concentration of hydrogen sulfide in a biogas.

***Please replace the paragraph on page 8, lines 12-13, with the following:***

~~Fig. 4 is a dot graph~~ Figs. 4(a) and 4(b) are dot graphs illustrating change with time in a COD removing rate.

***Please replace the paragraph on page 8, lines 14-16, with the following:***

~~Fig. 5 is a dot graph~~ Figs. 5(a) and 5(b) are dot graphs illustrating a relationship between concentration of hydrogen sulfide in a biogas and a COD removing rate in a biogas.

***Please replace the paragraph on page 11, lines 8-22, with the following:***

The reactor 4 is used after granular sludge comprising anaerobic bacteria is charged. The anaerobic treatment as a target of the invention targets anaerobic treatment in a temperature range of medium-temperature methane fermentation treatment wherein optimal temperature ranges from 30°C to 35°C and high-temperature methane fermentation treatment wherein optimal temperature ranges from 50°C to 55°C. Granular sludge comprising anaerobic bacteria is charged and a raw water (water to be treated) 1 is introduced from the liquid-transferring pipe 3 to the reactor 4. The raw water 1 is suitably diluted with a circulating liquid of treated water, water fed from the outside of the system, or the like, if necessary, and the flow rate of ~~inflow~~

~~water~~organic wastewater inside the reactor is controlled so as to be ~~from 0.5 to 5~~ between 0.5 and 5 m/h.

***Please replace the paragraph on page 19, lines 18-24, with the following:***

~~Fig. 3 shows~~Figs. 3(a) and 3(b) show concentration of hydrogen sulfide in a biogas in the methane fermenter, and ~~Fig. 4 shows~~ Figs. 4(a) and 4(b) show change in treatment results. ~~Fig. 5 shows~~ Figs. 5(a) and 5(b) show a relationship between concentration of hydrogen sulfide in the biogas and a $COD_{cr}$ removing rate. When the concentration of hydrogen sulfide in the biogas exceeds 3%, the $COD_{cr}$ removing rate remarkably decreased.

***Please replace the paragraph on page 20, lines 7-18, with the following:***

~~In Figs. 3 to 5, difference between examples cannot be clearly defined since the dots of respective Examples are gathered within the same area, but~~ In Fig. 3(a), it is revealed that the concentration of hydrogen sulfide in the biogas is 2% or less in every ~~Examples~~Example. Moreover, in Fig. ~~4,~~ 4(a) it is revealed that the $COD_{cr}$ removing rate is so high as 70% or more in every ~~Examples~~Example. Fig. ~~5~~ 5(a) is an integration of ~~Fig. 3 and Fig. 4~~ Fig. 3(a) and Fig. 4(a) and the dots of respective Examples are gathered in an extremely narrow area. This fact clearly shows that the concentration of hydrogen sulfide in the biogas is 2% or less in every ~~Examples~~ Example and thereby the $COD_{cr}$ removing rate reaches 70% or more.